

Design Project

Thermodynamics II

Dr. Crown

Mostafa Fath El-Den

Alex Marroquin

*Water reheat to expand in
one second stage turbine*

We modeled a steam powered power plant at 520°C and 10 MPa. Such power plant has an efficiency of 44.842%. After viewing which parameters could be changed, we decided to create 2 new models, one with optimized parameters and another with an additional reheat. Both are covered in the sections below.

Model 1: Original Power Plant

The original power plant is represented by the first model. It works at a high efficiency, 44.8%, and it produces a good amount of profit, approximately \$22 million. Regardless of this, the parameters are not optimized thus the plant is not producing as much profit as it could. This can be fixed by changing the initial temperature and pressure and by changing the percentage of feed water. In the next two models, two options are explored: higher initial temperature and pressure for greater work output, and an additional reheat before turbine 3 to increase the amount of work produced by that turbine.

Model 2: Optimized Parameters

In this model we decided to increase the temperature from 520°C to 600°C. The pressure was also increased from 10 MPa to 12 MPa. These values increased the efficiency from 44% to 47%. Considering coal costs the profits increased from \$22.3 million to \$27.5 million. This model does not provide as much profit as the third model but it does meet regulatory standards set by the government. CO₂ production is at a minimum which means less expense in filtering the pollutant out and no risk of fines.

↳ why do you say this? what is the reason?

Refer reader to explanation on ~~second~~ third model description

Model 3: Additional Reheat

In this model we added a reheat after turbine 2 before turbine 3 as shown in the figure below. This reheat increases the initial heat of the fluid before entering turbine 3 thus more work can be

produced than if the temperature remained at the same temperature of turbine 2 exit. The additional reheat both positive and negative consequences. The efficiency is reduced drastically, from 44% to about 28.94%. On the other hand the power output increases by a huge factor, from 85.515 MW to 141.145 MW. This in turn increases the profit from \$22 million to \$36 million including cost for coal used as fuel. This model is not intended as the main proposal; it only serves as an alternative to maximize profit regardless of efficiency. Although this model maximizes the profit it may have legal implications i.e. the low efficiency may produce more CO_2 gas pollutant which may exceed regulatory standards. The profit would still far exceed the profit of the original model even taking into account the expenses for filtering CO_2 but the government standards have to be taken into account.

Conclusion

Overall, model 3 provides the most profit with a low efficiency but environmental concerns have to be taken to account in addition to possible federal regulations. The most viable and safe option is model 2 which simply optimizes the parameters to produce the most work. This model has minimal environmental concerns and does not have any likelihood of violating any regulations. Depending on the area the plant is located and the regulations in that area, either of both models can be picked but the best choice overall would be model 2.

Exam Example Problem with isentropic efficiencies (eff_pump=90%, eff_turbine=85%)

State	Given	Find
#1	T= 520 P= 10000	H= 3424.484426 S= 6.66125196
#2s		
#2	P= 4000 S2= 6.661252	H= 3142.679281 S= 6.66125196
#3	T= 520 P= 4000	H= 3490.560945 S= 7.147701673
#4s		
#4	P= 500 S= 7.147702	H= 2898.041925 S= 7.1477
#5s		
#5	P= 8 S= 7.1477	H= 2236.616118 S= 7.1477
#6	P= 8 X= 0	H= 173.6315799 -----
#7s		
#7	P= 500 v= 0.001009	H= 174.1277875
#8	P= 500 X= 0	H= 639.7324329
#9s		
#9	P= 10000 v= 0.001453	H= 653.53508
#10	P= 10000 HX Bal.	H= 838.4843579
#11	P= 4000 X= 0	H= 1087.687306
#12	P= 500 H12= H11	H= 1087.687306

$m_{dot} =$	65 kg/s
$y' =$	9.00%
$y'' =$	14.07%

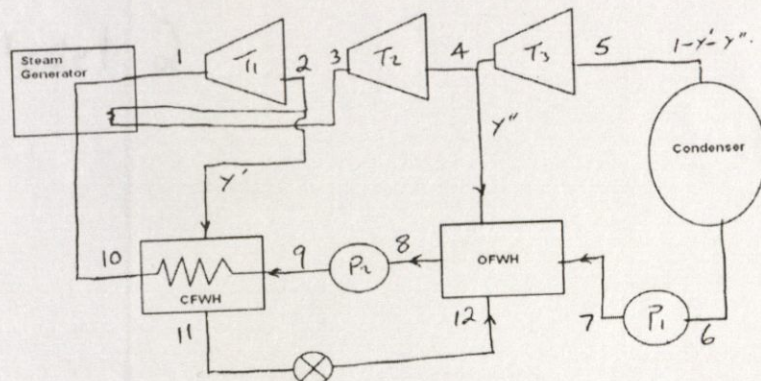
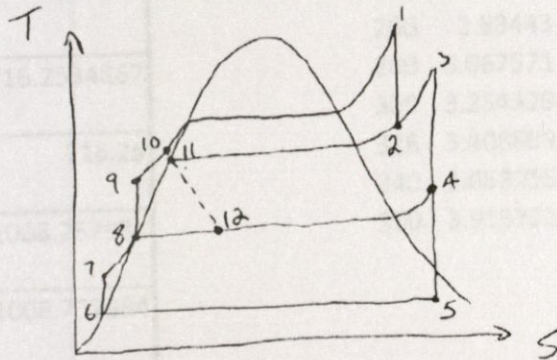
Wt1=	18317.33442 kW
Wt2=	35047.50003 kW
Wt3=	33072.22171 kW
Wp1=	-24.8110803 kW
Wp2=	-897.1720647 kW
Qin1=	168090.0045 kW
Qin2=	22612.30812 kW
Eff=	44.84217934 % ✓

Wtotal 85515.07301
Rate \$0.10
Profit per Day \$68,412.06
Profit per Year \$23,944,220.44

Coal 2460 kWh/ton
\$Coal \$16.67
Total Coal 97334.22944 ton
Total \$ Coal \$1,622,561.60

Actual Profit \$22,321,658.84

Where did you get this price?



Model 1

Profit per Day \$68,412.06
Coal 2460 kWh/ton
\$Coal \$16.67
Total Coal 97334.22944 ton
Total \$ Coal \$1,622,561.60
Actual Profit \$22,321,658.84

State	Given	Find
#1	T= 600 P= 12000	H= 3607.819932 S= 6.80275942
#2s		
#2	P= 3000 T= 366.4154	H= 3153.157407 S= 6.80275942
#3	T= 600 P= 3000	H= 3681.874836 S= 7.507660861
#4s		
#4	P= 709 T= 362.5085	H= 3189.25341 S= 7.5077
#5s		
#5	P= 8 T= 41.51129	H= 2349.881337 S= 7.5077
#6	P= 8 T= 41.51129	H= 173.6315799 S= 7.5077
#7s		
#7	P= 709 v= 0.001009	H= 174.3385749
#8	P= 709 X= 0	H= 699.0144041
#9s		
#9	P= 12000 v= 0.001527	H= 716.2534867
#10	P= 12000 HX Bal.	H= 716.25
#11	P= 3000 X= 0	H= 1008.757984
#12	P= 500 H12= H11	H= 1008.757984

m_dot=	65
y'=	0.00%
y''=	17.40%

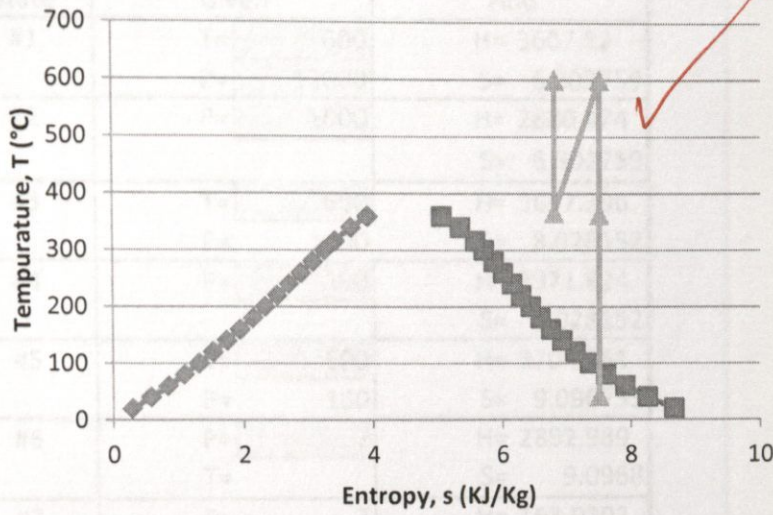
Wt1=	29553.06 kW
Wt2=	32020.39 kW
Wt3=	45064.43 kW
Wp1=	-37.9573 kW
Wp2=	-1120.54 kW
Qin1=	187951.8 kW
Qin2=	34366.63 kW
Eff=	47.44518 % ✓

Temp	s_f	s_g
20	0.292811	8.666387
40	0.571146	8.256159
60	0.832346	7.908735
80	1.077178	7.611366
100	1.307965	7.354042
120	1.527455	7.128783
140	1.738025	6.929064
160	1.941414	6.749365
180	2.138731	6.584897
200	2.330691	6.43144
220	2.518075	6.285232
240	2.702054	6.142853
260	2.88443	6.000998
280	3.067571	5.856055
300	3.254329	5.703215
316	3.408809	5.570101
340	3.658015	5.333203
360	3.913722	5.04852

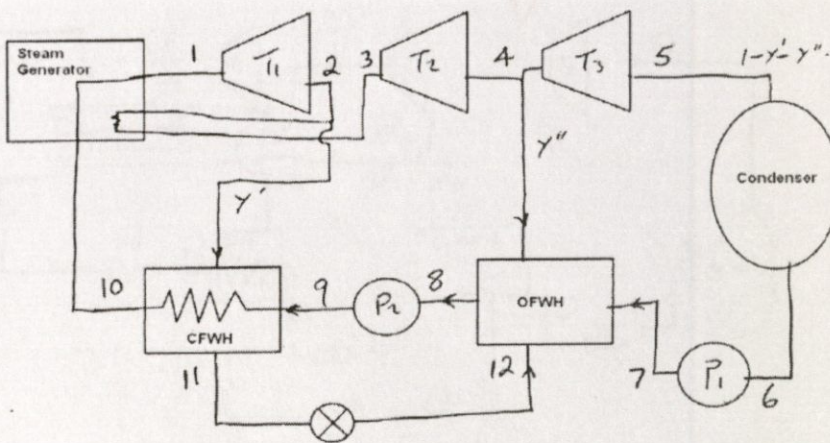
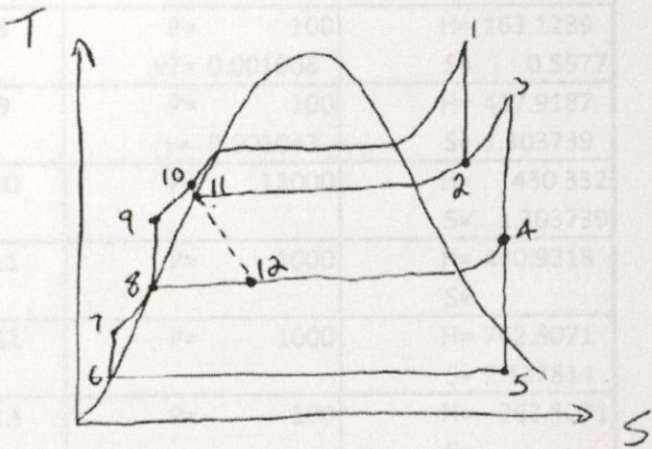
Wtotal= 105479.3863
 Rate \$0.10
 Profit per Day \$84,383.51
 Profit per Year \$29,534,228.17
 Coal 2460
 \$Coal \$16.67 kWh/ton
 Total Coal \$120,057.84
 Total \$ Coal \$2,001,364.16 ton
 Actual Profit \$27,532,864.01

Model 2

Temperature Vs. Entropy



Stage	Temp	S
1	600	6.802759
2	366.4154	6.802759
3	600	7.507661
4	362.5085	7.5077
5	41.51129	7.5077



State	Given	Find
#1	T= 600 P= 12000	H= 3607.82 S= 6.802759
#2	P= 1000	H= 2880.474 S= 6.802759
#3	T= 600 P= 1000	H= 3697.396 S= 8.028152
#4	P= 100	H= 2971.624 S= 8.028152
#5	T= 600 P= 100	H= 3704.261 S= 9.096753
#6	P= 7 T= 39.00202	H= 2892.989 S= 9.0968
#7	P= 7	H= 163.0302 S= 0.557671
#8	P= 100 v7= 0.001008	H= 163.1239 S= 0.5577
#9	P= 100 v= 0.001043	H= 417.9187 S= 1.303739
#10	P= 12000	H= 430.332 S= 1.303739
#11	P= 1000	H= 440.9218 S=
#12	P= 1000	H= 762.5071 S= 2.137814
#13	P= 100	H= 762.5071 S=

m_dot=	65 kg/s
P(y')=	1000
y'=	0.50%
y''=	8.97%

Wt1=	47277.50428 kW
Wt2=	46939.31199 kW
Wt3=	47741.24965 kW
Wp1=	-5.514393038 kW
Wp2=	-806.8640252 kW
Qin1=	238689.1373 kW
Qin2=	43113.78102 kW
Qin3=	205848.3767 kW
Eff=	28.94397881 %

Carnot % 64.26%

Wtotal = 141145.6875

Rate \$0.10

Profit per Day \$112,916.55

Profit per Year \$39,520,792.50

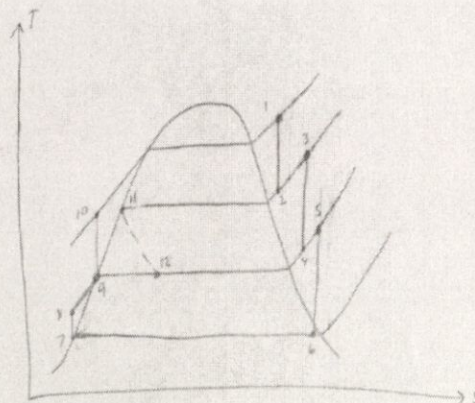
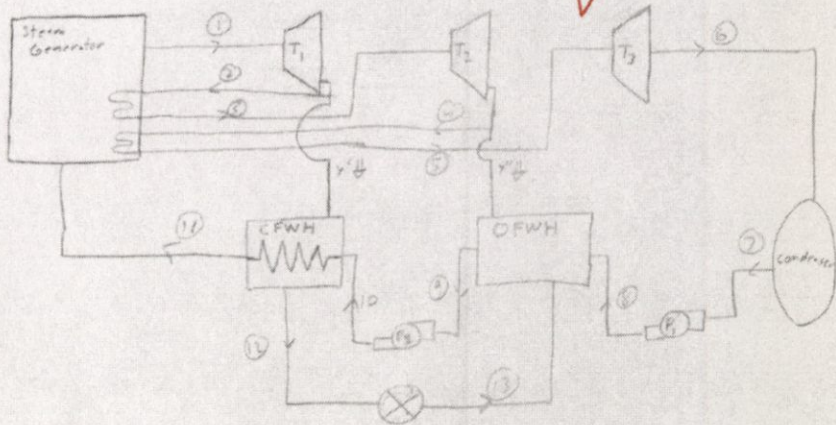
Coal 2460 kWh/ton

\$Coal \$16.67

Total Coal 160653.6281 ton

Total \$ Coal \$2,678,095.98

Actual Profit \$36,842,696.52



Model 3

$$\eta = \frac{\sum W}{\sum Q_n}$$

$$\eta = \frac{h_1 - h_2 + (1 - \gamma')(h_3 - h_4) + (1 - \gamma' - \gamma'')(h_5 - h_6) + (1 - \gamma' - \gamma'')(h_7 - h_8) + h_9 - h_{10}}{(1 - \gamma')(h_3 - h_2) + (1 - \gamma' - \gamma'')(h_5 - h_4) + h_1 - h_{11}}$$

$$\eta = \frac{h_1 - h_2 + (1 - \gamma')(h_3 - h_4) + (1 - \gamma' - \gamma'')(h_5 - h_6 + h_7 - h_8) + h_9 - h_{10}}{(1 - \gamma')(h_3 - h_2 + h_5 - h_4) + \gamma''(h_5 - h_4) + h_1 - h_{11}}$$

$$\eta = \frac{h_1 - h_2 + (1 - \gamma')(h_3 - h_4) + (1 - \gamma' - \gamma'')(h_5 - h_6 + h_7 - h_8) + h_9 - h_{10}}{(1 - \gamma')(h_3 - h_4) + (1 - \gamma')(h_5 - h_2) + \gamma''(h_5 - h_4) + h_1 - h_{11}}$$

↑ Factors to increase	No Effect	↓ Factors to decrease
h_4 h_7 h_9 h_{11}	h_1 h_3	h_2 h_5 h_6 h_8 h_{10}

Mostafa Fath El-Den

Alex Merquin